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Corrosion Resistance of Selected Ceramic Materials to Sulfuric Acid

By James P. Bennett



UNITED STATES DEPARTMENT OF THE INTERIOR

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	UNIT OF MEASURE ABBREVIATIONS	USED IN TH	IS REPORT
°C	degree Celsius	min	minute
g/cm ³	gram per cubic centimeter	mm	millimeter
h	hour	pct	percent
in	inch	psi	pound per square inch
L	liter	wt pct	weight percent

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CORROSION RESISTANCE OF SELECTED CERAMIC MATERIALS TO SULFURIC ACID

By James P. Bennett¹

ABSTRACT

The Bureau of Mines is investigating the acid resistance of ceramic materials to identify construction materials for emerging technology in chemical and metallurgical processes. Eight commercial ceramic materials, were evaluated: two red shale, two fireclay, one silicon carbide, one silica, one carbon, and one high-alumina. Samples were exposed to 10 wt pct H_2SO_4 at 50° C and 10, 30, 50, 70, and 90 wt pct H_2SO_4 at 90° C for time periods of 110 days. Statistically significant changes in cold crushing strength were observed in the silicon carbide and carbon materials. Weight changes and the leach rate of A1, Ca, Fe, K, Mg, Na, Si, and Ti were also monitored.

The most severe corrosion conditions were at 90° C and 30 to 50 wt pct H_2SO_4 for the acidproof and at 10 wt pct H_2SO_4 for the acid-resistant materials. The silica and the high-alumina materials were the most acid-resistant, followed by the higher density red shale and fireclay.

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Extensive literature, published during recent years, identifies three general methods of fine-particle preparation (1):² (1) solution techniques, (2) vapor-phase techniques, and (3) salt decomposition techniques. Solution techniques, also referred to as "chemical" preparation (2), offer the advantages of ease of preparation, good control of composition, and homogeneity. Among the solution techniques a number of terms, such "codecomposition" (3), "evaporative as decomposition from solutions" (EDS) (4-5), "citrate process" (6), and "alkoxide process" (7) are frequently encountered.

Vapor-phase techniques are receiving more and more attention, due mostly to interest in high-performance structural ceramics such as SiC and Si₃N₄. These techniques lead to unaggregated powders. Among the techniques in this category are all plasma methods ($\underline{8-9}$) and others involving gaseous reactants.

Decomposition of precursor salts (e.g., oxalates) has been employed in the preparation of fine-powder carbides (10-11).

BN powders have been prepared by the reaction of boron oxides and borates with ammonium chloride (NH_4Cl) in N₂ and NH₃ atmospheres (12). In certain reactions, in order to increase the reaction rates in the solid state, that is, to effectively increase the reaction surface areas, inert fillers such as CaCO₃ and calcium phosphates have also been employed (13). Ammonium salts other than NH₄Cl have also been used in BN synthesis.

Ammonium thiocyanate, for example, resulted in much higher reaction rates with boric acid in the BN synthesis (14).

Among the less conventional laboratory techniques reported for the preparation of nonoxide ceramic powders are the reaction of compounds (such as silanes, boranes, and halides) containing the desired cations in super-high-frequency discharge plasma (15), chemical vapor deposition techniques (16-22), and the use of laser energy (23). Similar reactions have also been studied employing conventional high-temperature furnaces at 1,500° to 1,900° C (24-27).

Production of complex nitride powder has been studied by the nitridation of metal halides (SiCl₄, BCl₃) in an N plasma (15). Chemical vapor deposition techniques have also been used to prepare thin films of BN, Si₃N₄, and TiN (8-12). Extremely fine, uniform Si₃N₄ and SiC powders have been synthesized from SiH₄, NH₃, and C₂H₄ gas-phase reactants heated by a CO₂ laser (23). Nitrides of Si, B, and Ti have also been prepared by the reaction of their halides with ammonia or ammonia salts at high temperatures (24-27).

No mention of preparing BN from halides of B with the reaction of ammonia salts or ammonia in the liquid phase has been made in the literature. In view of this finding, research efforts included a study of obtaining ultrafine BN powders from the reactions of halides with NH₄Cl and NH₃ in the liquid phase.

EXPERIMENTAL EQUIPMENT AND PROCEDURES

REACTIONS BETWEEN 500° AND 750° C

Two different approaches were evaluated for the synthesis of fine BN powders. The first was the reaction between an inorganic B compound and an organic N compound between 500° and 750° C in an NH₃ atmosphere. For this a hightemperature controlled-atmosphere furnace

 2 Underlined numbers in parentheses refer to items in the list of references at the end of this report.

was used. Inorganic B compounds used included boric oxide (B_2O_3) , boric acid (H_3BO_3) , borax $(Na_2B_4O_7 \cdot 10H_2O)$, and anhydrous sodium tetraborate $(Na_2B_4O_7)$. Carbimide $(NH_2 \cdot CO \cdot NH_2)$ and thiocarbimide $(NH_2 \cdot SO \cdot NH_2)$ were used as N_2 sources. The powdered reactants were mixed in stoichiometric proportions and placed in the furnace. The furnace chamber was evacuated and purged with NH3 gas before the temperature was raised. Experiments ran from 4 to 24 h at 500° to 750° C.

REACTIONS BETWEEN -75° AND 200° C

The second approach involved the synthesis of BN through reactions between various N and B compounds leading to the formation of possible elemento-organic compounds as intermediate precursor species, the decomposition of which might lead to BN formation. Such compounds included NH₃, boron halides (principally boron trichloride, BCl₃), ammonium chloride (NH₄Cl), and sodium borohydride (NaBH₄).

For the second approach, material preparation and handling procedures were performed in a dry-box system, a simplified schematic of which is shown in figure 1. The atmosphere in the box was maintained by a VAC Dri-train³ unit capable of generating an inert gas atmosphere containing less than 1 ppm 0_2 and/or moisture. This high-purity inert atmosphere was obtained by circulating the gas in a closed system going through a purifying chamber equipped with molecular sieves to trap 0_2 and moisture. Figure 2 shows the dry-box assembly. Reactions were carried out in the experimental unit (fig. 3) consisting of a three-necked, 500-mL glass reaction vessel and a small vacuum system with cold traps.

Three systems were studied. They included ammonia-boron halide, ammonium salt-boron halide, and ammonium saltmetal borohydride reactions.

³Reference to specific products does not imply endorsement by the Bureau of Mines.



FIGURE 1. - Simplified schematic of Dri-train equipment.



FIGURE 1. - Construction detail of reaction vessel.



ACIDPROOF MATERIALS

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Statistically significant⁴ weight changes occurring in the acidproof materials are listed in table 2. All materials showed an increase in weight loss in 10 wt pct H_2SO_4 when the temperature was increased from 50° to 90° C. At 90° C, the materials showed an increase in weight loss with an increase in acid concentration up to either 30 or 50 wt pct H_2SO_4 , and then a decrease in weight losses at 70 wt pct. At 90 wt pct H_2SO_4 , all samples showed a weight gain. Red

⁴Statistically significant changes (Student's t-test) at a 99-pct confidence level, compared with data for untreated specimens $(\underline{15})$.

shale A and fireclay B samples, which have the highest apparent porosity of the acidproof materials, have the highest weight losses, of 8.11 and 7.29 wt pct, respectively, when exposed to 50 wt pct H_2SO_4 at 90° C. The largest weight losses for the low-porosity red shale B (0.46 pct) and fireclay A (1.54 pct) materials occurred in 30 wt pct H_2SO_4 at 90° C.

Cold crushing strength data for the acidproof materials are listed in table 3. No discernible trends were observed for any of the red shale or fireclay samples and no significant differences exist between cold crushing strength values of the top (vapor exposed) and the bottom (liquid exposed) halves of the test samples.

Exposure conditions ¹	Red s	hale	Fireclay			
	A	В	Α	В		
50° C, 10 H ₂ SO ₄	*-0.50±0.06	*-0.08±0.05	*-0.24±0.04	*-0.54±0.03		
90° C, 10 H ₂ SO ₄	*-1.16± .13	*24± .10	*58± .11	*-3.05± .10		
90° C, 30 H ₂ SO ₄	*-5.31±.61	*46± .13	*-1.54± .19	*-6.35±.36		
90° C, 50 H ₂ SO ₄	*-8.11±.30	*18± .01	*-1.03± .15	*-7.29±.23		
90° C, 70 H ₂ SO ₄	*-1.35± .14	*21± .04	*.56± .08	25±.27		
90° C, 90 H ₂ SO ₄	*.87±.23	*1.17±.21	*1.73± .12	*6.06±.28		

TABLE 2. - Changes in weight of acidproof materials exposed to $\rm H_2SO_4$ for 110 days, percent

¹H₂SO₄ in weight percent.

*Statistically significant change at 99-pct confidence level, compared with data for untreated specimen (Student's t-test).

NOTE.--Plus-minus (±) values are at 95-pct confidence intervals.

TABLE 3. - Cold crushing strength of acidproof materials exposed to $\rm H_2SO_4$ for 110 days, pound per square inch

Exposure conditions ¹	Red s	hale	Fireclay			
	A	В	Α	В		
Unexposed	18,800±1,500	20,300±1,700	9,800±1,300	9,700± 700		
Top: ²						
50° C, 10 H ₂ SO ₄	26,500±1,900	20,300±1,000	*6,700± 800	*14,400±1,200		
90° C, 10 H ₂ SO ₄	18,500±1,900	$17,700\pm 2,100$	10,200±1,200	*14,400± 900		
90° C, 30 H ₂ SO ₄	15,200±2,600	17,800±2,200	*6,700±1,000	*5,900± 500		
90° C, 50 H ₂ SO ₄	*22,700±1,700	*17,300±1,200	9,200± 900	8,700± 700		
90° C, 70 H ₂ SO ₄	19,900±1,600	*27,100±1,400	11,100±1,200	*14,000±1,400		
90° C, 90 H ₂ SO ₄	*25,000±1,600	*25,600±1,800	9,900±1,100	*13,800±1,300		
Bottom: ³						
50° C, 10 H ₂ SO ₄	*23,400±2,000	18,500±1,400	*6,400± 900	*13,600±1,100		
90° C, 10 H ₂ SO ₄	16,000±1,700	*16,500±1,900	9,100±1,000	*13,000± 800		
90° C, 30 H ₂ SO ₄	*11,000±1,600	18,800±1,700	*6,300± 900	*5,100± 300		
90° C, 50 H ₂ SO ₄	20,900±2,500	*10,700± 800	*13,800±1,000	*7,500± 700		
90° C, 70 H_2SO_4	19,300±1,300	*25,700±1,600	11,100±1,600	*12,000±1,000		
90° C, 90 H ₂ SO ₄	*24,600±1,500	*26,700±1,300	10,700±1,300	*16,700±1,300		

 $^{1}\text{H}_{2}\text{SO}_{4}$ in weight percent. ^{2}Top half of sample, exposed to gas phase.

³Bottom half of sample, exposed to H_2SO_4 solution.

*Statistically significant change at 99-pct confidence level, compared with data for untreated specimen (Student's t-test).

NOTE.--Plus-minus (±) values are at 95-pct confidence intervals.

The weight percent of ions leached from the acidproof materials are listed in table 4. Silicon was leached from samples in 10-pct-H₂SO₄ concentrations and, except for one instance, was not removed at higher acid concentrations. Calcium was removed in trace amounts (less than 0.033 pct) in all acid concentrations. As temperature or acid concentration was increased, less calcium was removed. All other ions exhibited an increase in quantity leached from the samples with an increase in temperature at the same acid concentration. As acid concentration was increased from 10 to 90 pct at 90° C, the quantity of ions removed from a material increased to a maximum value at either 30 or 50 wt pct H_2SO_4 , then decreased with atmosphere with reaction times of 24 h or longer, formation of BN was observed. This reaction, however, was low yielding, probably owing to the decreased reactive surface area of the boric anhydride upon melting at 450° C. To increase the yield, the effective surface area of the boric acid was increased by the addition of tricalcium phosphate (Ca₃(PO₄)₂) as an inert filler. This resulted in BN yields as high as 75 pct for reaction times of 24 h. The synthesis process may be represented by the following reaction:

$$B_2O_3 + NH_2 \cdot CO \cdot NH_2 \xrightarrow{750^\circ C} 2BN + CO_2$$

+ 2H_2O. (1)

When borax and carbimide were used as reactants in an NH₃ atmosphere, BN formation proceeded much faster than in the boric acid-carbimide system. The reaction could be represented by--

$$Na_{2}B_{4}O_{7} \cdot 10H_{2}O + 2NH_{2} \cdot CO \cdot NH_{2} \xrightarrow{750^{\circ} C} 4BN$$

$$+ Na_{2}O + 2CO_{2} + 14H_{2}O. \qquad (2)$$

Reaction products obtained were washed in dilute HCl, and the insoluble portion was filtered out. X-ray diffraction (XRD) analysis of the filtered powder indicated that it was amorphous. Heat treatment of this material at 1,400° C in an N₂ atmosphere for several hours resulted in crystalline BN powder based on XRD patterns. The BN yield of reaction 2 was as high as 95 pct of expected theoretical value. Tt appears that dehydration of borax at temperatures (200° to 400° C) below the reaction temperature results in a spongelike anhydrous borax with a very high surface area. This, along with the decomposition of the carbimide to produce additional NH3 gas of high reactivity, results in higher BN yields.

The same reaction run in an N_2 atmosphere resulted in lower yields. The higher yields produced in an NH_3 atmosphere compared to an N_2 atmosphere may be due to the higher reactivity of N_2 produced by NH_3 decomposition at 450° C.

The H_2 produced as a result of NH_3 decomposition might also have a catalytic effect on the reaction, resulting in higher yields.

The use of thiocarbimide (NH_2SONH_2) as the organic N₂ source further increased the reaction rate, as evidenced by the shorter time required for the reaction to reach completion. In the reaction with thiocarbimide, sodium sulfides were produced as potential reaction byproducts, which may further decompose at about the reaction temperature of 750° C. This decomposition process at the BN-formation temperature results in spongelike highsurface-area material, thus accelerating the reaction rates.

REACTIONS BETWEEN -75° AND 200° C

Ammonia-Boron Halide Reactions

Once the reactants (NH₃ and BCl₃) are introduced into the three-neck reaction flask, reaction starts immediately, as evidenced by formation of a white powder around the walls of the reaction flask. This reaction is allowed to continue for 2 to 3 h. At the end of such time the excess liquid NH₃ remaining in the flask is removed by vacuum, the white powdered reaction product is isolated and dried at room temperature. The following two reactions appear to take place either concurrently or consecutively:

 $\begin{array}{rcl} & \text{6NH}_3 & (\text{liquid}) + \text{BCl}_3 & (\text{liquid}) \\ & & -75^\circ & \text{C} \\ & \longrightarrow & \text{B(NH}_2)_3 + 3\text{NH}_4\text{Cl}, \end{array}$

 $3NH_3$ (liquid) + $3BCl_3$

$$\xrightarrow{-75^{\circ}} C \xrightarrow{-75^{\circ}} C1_3 \cdot B_3 \cdot N_3 \cdot H_3 + 6HC1.$$
(4)

The intermediate reaction products, elemento-organic BN compounds, that may be formed in these reactions have not been isolated and identified. The general chemistry of these systems, however, suggests the formation of such compounds and the precipitation of BN as a result of their carbothermic decomposition. An attractive feature of these reactions appears to be their general applicability to the preparation of other nitrides, such as AlN, TiN, and Si_3N_4 . Future efforts should be directed toward a study of the reaction mechanisms through the isolation and characterization of the intermediate precursor compounds. Understanding these reactions would help determine the feasibility of the formation of other nitride compounds at low temperatures.

XRD analysis of the dried material identified the presence of NH_4 Cl in reaction 3; detection of HCl fumes through the mercury bubbler in the reaction set confirmed reaction 4.

The rest of the powder in the reaction products was amorphous to X-rays. After being heated in vacuum at 200° to 250° C for several hours, the powder was still amorphous to XRD. Heat treatment of the powder at 1,200° to 1,400° C for several hours resulted in BN detectable A chemical analysis of the by XRD. powder after washing in dilute HCl acid solution and filtration revealed 42.4 pct B, 53.1 pct N, and 0.7 pct 0. Low 02 content of the sample illustrates the appropriateness of the method for preparing high-chemical-purity BN compared to borax technique ($0_2 \cong 5$ pct). Surface area of BN powder prepared by this method was measured to be 80 to 100 m^2/g depending on the temperature of crystallization. Surface area and particle size of a commercially available BN powder were determined to be $10 \text{ m}^2/\text{g}$ and 45 µm, respectively. Densities (helium pycnometer) were 2.18 to 2.21 g/cm³.

Ammonium Salt-Boron Halide Reactions

As previously described the reaction was allowed to proceed for 8 to 12 h. The flask was then cooled to room temperature, and the organic solvent was removed by vacuum followed by heating the solid residue in vacuum to 200° to 250° C for several hours. XRD analysis of reaction product(s) showed an amorphous component and NH₄Cl. Further heat treatment of this powder at 1,200° to 1,400° C in vacuum or N₂ atmosphere resulted in BN powder detectable by XRD. A possible reaction sequence may be--

$$3NH_4C1 + 3BC1_3 \xrightarrow[Benzene]{\sim 80^{\circ} C} C1_3 \cdot B_3 \cdot N_3 \cdot H_3$$

+ 9HC1, (5)

then, upon heating in vacuum at approximately 250° C,

$$C1_3 \cdot B_3 \cdot N_3 \cdot H_3 \xrightarrow{\Delta} 3BN + 3HC1.$$
 (6)

Elemental analysis of the BN thus obtained gave 42.8 pct B, 54.1 pct N, and 2.5 pct O, which is similar to the composition of the BN powder from the ammoniaboron halide reaction and compares favorably with theoretical composition of BN (B/N = 0.79).

Surface area and density measurements gave values ranging from 80 to $110 \text{ m}^2/\text{g}$ and 2.15 to 2.20 g/cm³, respectively.

White powder formed by the NH_4C1 + NaBH4 reaction was isolated upon the removal of organic solvent by vacuum and heating of the sample to 200° to 250° C under vacuum for several hours. As with the two previous reaction systems, this powder was amorphous to X-rays; only upon heat treatment at 1,200° to 1,400° C in vacuum or N₂ for several hours was BN detected by XRD analysis.

Chemical analysis of the powder showed 42.0 pct B, 52.7 pct N, and 2.3 pct O, which again compared well with the theoretical BN composition and the powder from the other two reaction systems described.

Values of 70 to $200 \text{ m}^2/\text{g}$ and 2.15 to 2.22 g/cm³ were obtained for the surface area and density, respectively.

In addition to surface area, density and elemental analysis attempts were made to measure the particle size by direct methods; namely, by scanning electron microscope (SEM) and X-ray linebroadening techniques.

TABLE 5	Changes	in we	ight of	acid-resistant	materials	exposed
to H ₂ SO ₄	for 110	days,	percent	t		

Exposure conditions ¹	SiC	Silica	Carbon	High	
				alumina	
50° C, 10 H ₂ SO ₄	*-0.37±0.05	*-0.45±0.02	*-0.10±0.05	*-0.12±0.01	
90° C, 10 H ₂ SO ₄	*40± .04	*31± .03	*63± .01	*16± .01	
90° C, 30 H ₂ SO ₄	*40± .08	*27± .01	*32±.06	*10± .01	
90° C, 50 H ₂ SO ₄	*25±.04	*21± .01	*11± .03	*02± .01	
90° C, 70 H ₂ SO ₄	*30± .01	*33± .03	*1.31± .12	*10± .01	
90° C, 90 H ₂ SO ₄	*23± .03	08± .14	*2.59±.06	01± .01	

¹H₂SO₄ in weight percent.

*Statistically significant change at 99-pct confidence level, compared with data for untreated specimen (Student's t-test).

NOTE.--Plus-minus (±) values are at 95-pct confidence intervals.

TABLE 6. - Cold crushing strength of acid-resistant materials exposed to H₂SO₄ for 110 days, pound per square inch

Exposure conditions ¹	SiC	Silica	Carbon	High
				alumina
Unexposed	14,400±1,000	4,100±300	8,000±500	58,500±8,100
Top: ²		1		
50° C, 10 H ₂ SO ₄	*9,700± 800	4,200±400	*6,500±400	*80,800±7,300
90° C, 10 H ₂ SO ₄	*11,500±1,000	4,100±300	*6,600±500	63,000±7,800
90° C, 30 H ₂ SO ₄	*11,300± 600	3,600±300	*5,700±400	*84,400±6,700
90° C, 50 H ₂ SO ₄	14,000± 900	*4,700±300	8,200±400	66,200±7,200
90° C, 70 H ₂ SO ₄	15,400±1,200	3,800±300	*6,800±500	*79,800±6,200
90° C, 90 H ₂ SO ₄	13,100± 800	4,200±200	*6,700±400	*76,200±7,600
Bottom: ³				
50° C, 10 H ₂ SO ₄	*8,800± 900	4,300±300	*6,400±500	*76,700±7,400
90° C, 10 H ₂ SO ₄	*10,300± 800	4,300±200	*6,600±600	58,500±8,300
90° C, 30 H ₂ SO ₄	*12,400±1,100	3,900±300	*5,500±300	*75,200±5,400
90° C, 50 H ₂ SO ₄	13,200± 900	*4,700±300	8,200±300	68,000±7,100
90° C, 70 H ₂ SO ₄	14,400±1,000	3,800±300	*6,800±500	*76,500±6,000
90° C, 90 H ₂ SO ₄	13,400±1,000	4,400±200	*6,800±500	68,100±7,600

¹H₂SO₄ in weight percent.

²Top half of sample, exposed to gas.

³Bottom half of sample, exposed to H₂SO₄ solution.

*Statistically significant change at 99-pct confidence level, compared with data for untreated specimen (Student's t-test).

NOTE.--Plus-minus (±) values are at 95-pct confidence intervals.

and acid concentrations, but showed a weight increase at 90° C in 70 and 90 wt pct H_2SO_4 , reaching a maximum value of 2.6 wt pct in 90 wt pct H_2SO_4 . The reason for these weight increases has not been determined.

Cold crushing strength values are listed in table 6 for the acid-resistant materials. A statistically significant decrease in crushing strength from 8,000 to about 6,500 psi occurred in the carbon material at all acid concentrations and temperatures, except at 50 wt pct H_2SO_4 and 90° C. The SiC material had a statistically significant decrease in crushing strength from 14,400 to about 11,000 psi that occurred in 10 wt pct H_2SO_4 at 50° C and 10 and 30 wt pct H_2SO_4 at

90° C. The high-alumina and silica samples show no statistically significant strength losses.

The weight percentages of ions removed from the acid-resistant materials exposed to H_2SO_4 for 110 days are listed in table 7. During the 110-day leach, the ion removal rate from the four acid-resistant materials tended also to fit the secondorder parabolic equation described in the "Acidproof Materials" section, with 94 out of 152 curves yielding coefficients of correlation above 0.95. The quantity of ions removed from samples generally decreased when acid concentration was increased from 10 to 90 wt pct H_2SO_4 at 90° C. The quantity of ions removed from samples exposed to 10 wt pct H_2SO_4 did not show a trend when temperature was increased from 50° to 90° C. In all acidresistant materials, either the Al or Fe ions were leached in the largest quantities. The greatest amount of a single ion removed (0.24 pct Fe) occurred in the SiC material at 50° C and 10 wt pct H_2SO_4 . All other ions were leached in quantities less than 0.07 pct.

The total ion leach data for the acidresistant materials are shown in figure 3. All samples shown have a decrease in the total ions removed when acid concentration was increased from 10 to 90 pct at 90° C, with no ions removed in 90 pct H_2SO_4 . The SiC and the high-alumina samples show a decrease in the total quantity of ions leached in 10 wt pct H_2SO_4

TABLE	7.	-	Ions	leached	in	110	days	from	acid-resistant	materials,	weight	percent
-------	----	---	------	---------	----	-----	------	------	----------------	------------	--------	---------

Mate	rial and	[Ion leached							
exposure	conditions ¹	Al	Ca	Fe	K	Mg	Na	Si	Ti	ions
-										leached
SiC:	anan anan israe rapa kaninan senerara aran aran senerara.		7							
50°C,	10 H ₂ SO ₄	0.0190	0.0058	0.243	0.0018	0.0023	0.0004	0.0095	0.0408	0.323
90°С,	$10 H_2 SO_4$.0229	.0034	.232	.0017	.0020	.0008	.0025	.0248	.290
90°C,	30 H ₂ SO ₄	.0178	.0014	.201	.0008	.0008	.0006	.0016	.0267	.250
90°С,	50 H ₂ SO ₄	.0119	.0008	.078	.0005	.0007	.0002	ND	.0316	.124
90°С,	70 H ₂ SO ₄	.0047	.0006	.017	.0002	.0001	.0001	ND	.0188	.042
90°C,	90 H ₂ SO ₄	.0003	.0002	.004	ND	ND	ND	ND	.0053	.010
Silica:										
50°C,	$10 H_2SO_4 \dots$.0300	.0143	.0542	.0056	.0109	.0009	.0117	.0006	.128
90°С,	$10 H_2SO_4$.0354	.0098	.0617	.0093	.0109	.0021	.0090	.0009	.139
90°C,	30 H ₂ SO ₄	.0279	.0093	.0478	.0056	.0122	.0018	ND	.0008	.105
90°С,	50 H ₂ SO ₄	.0220	.0061	.0330	.0038	.0053	.0016	ND	.0010	.073
90°С,	70 H ₂ SO ₄	.0174	.0055	.0224	.0017	.0047	.0013	ND	.0006	.054
90°С,	90 H ₂ SO ₄	.0020	.0019	.0047	.0013	.0017	.0005	ND	ND	.012
Carbon:										
50°C,	$10 H_2 SO_4 \dots$.0017	.0017	.0116	.0004	.0005	.0004	ND	ND	.0163
90°C,	$10 H_2SO_4 \dots$	•0048	.0015	.0182	.0014	.0014	.0024	.0072	.0001	.0290
90°С,	$30 H_2SO_4 \dots$.0030	.0018	.0141	.0002	.0006	.0023	.0025	.0001	.0246
90°С,	50 H ₂ SO ₄	.0018	.0008	•0079	.0001	.0006	.0011	ND	.0002	.0125
90°С,	70 H ₂ SO ₄	.0010	.0008	.0055	ND	ND	.0011	ND	ND	.0084
90°С,	90 H ₂ SO ₄	.0001	ND	.0003	ND	ND	.0005	ND	ND	.0009
High alu	nina;									
50°C,	$10 H_2SO_4$.0373	.0143	.0004	.0003	.0017	.0033	·•0078	.0001	.0652
90°С,	$10 H_2SO_4 \dots$.0332	.0080	.0004	.0006	.0026	.0037	.0096	.0004	•0585
90°С,	30 H ₂ SO ₄	.0299	.0043	.0004	.0004	.0027	.0029	ND	.0002	•0408
90°С,	50 H ₂ SO ₄	.0025	.0005	ND	ND	.0004	.0002	ND	ND	.0036
90°С,	70 H ₂ SO ₄	.0197	.0031	,0002	ND	.0022	.0012	ND	ND	.0264
90°С,	90 H ₂ SO ₄	ND	ND	ND	ND	ND	ND	ND	ND	ND

ND Not detected.

¹H₂SO₄ in weight percent.



FIGURE 3. - Total ions leached from acid-resistant materials in 110 days of H₂SO₄ exposure.

when temperature was increased from 50° to 90° C, and the silica and the carbon showed an increase. The largest amount of total ions leached, 0.32 pct, occurred in the SiC material exposed to 10 wt pct H₂SO₄ at 50° C. The carbon and high-alumina samples had the least total ions leached. Less than 0.03 wt pct of total ions was leached from the carbon and less than 0.07 wt pct from the high-alumina samples under the conditions studied.

Scanning electron microscopy, electron probe, and XRD examinations of the acidresistant materials indicated no phase changes occurred. No correlation existed between ion leaching and cold crushing strength values. The carbon material, which had nearly a continual strength decrease under the conditions investigated, had the lowest total ion removal of any material tested.

CONCLUSIONS

Samples of two red shale, two fireclay, one SiC, one silica, one carbon, and one high-alumina ceramic materials were exposed to 10 wt pct H_2SO_4 for 110 days at 50° C, and to 10, 30, 50, 70, and 90 wt pct H_2SO_4 for 110 days at 90° C. A study of the corrosion effects after this 110-day period of exposure to H_2SO_4 produced the following indications:

1. The silica and the high-alumina samples had the best acid-resistance properties.

2. Total ions 1eached and sample weight loss values were generally highest at exposures of 30 to 50 wt pct H_2SO_4 at 90° C for the acidproof materials and at 10 wt pct H_2SO_4 for the acid-resistant materials.

3. The highest density red shale and fireclay materials had good acid-resistance properties, with a maximum total ion

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4. In general, the Fe and Al ions had the highest removal rates. while removal of Ca, Mg, Na, K, and Ti ions removal was minor.

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